Solutions for Performance Monitoring, Diagnosis and Optimization of Power Plants
Agenda

- Introduction
- Carbon-in-Ash Instrument
- Mill Runback Calculator
- Combustion Optimization
- Soot Blowing Optimization
- Startup Optimization
- Life-time Calculation
- Temperature State Space Control
- Life Steam Flow Calculation
- Unit Control
- Energy Optimizer
- Process Quality Monitoring
- Loop Performance Monitoring
- Energy Efficiency Consulting
Only 20% of primary energy generates economic value. The rest is lost to conversion processes, transportation and operational inefficiencies.
Motivation for optimization

**Benefits**
- Reduce fuel consumption and emissions
- Increase flexibility
- Identify and rectify equipment problems
- Improve predictive maintenance and availability
- Optimize asset lifecycles

**Measures**
- Tune control loops
- Optimize the combustion process and improve boiler controls
- Optimize ramp rates, low load running and startups
- Optimize operation of multiple generating units
- Monitor and predict plant performance
- Issue early warnings for equipment diagnosis and preventive maintenance
Carbon In Ash Instrument Basics

- Majority of the combustible portion of the ash accounting for the energy loss is simply unburned carbon.

- Unburned carbon is a highly variable parameter which is dependent upon coal type, load, fuel and air distribution, and other boiler-specific factors, the need for on-line real-time measurement has become more critical in combustion optimization process

- ABB Carbon In Ash Instrument (CIA) provides a true real-time and representative measurements of the unburned carbon in the fly ash for utility power plants
Carbon In Ash Instrument
ABB’s Technology Edge!

- Active Component is a 94GHz Microwave System
- Slightly Parabolic “Mirrors” Create Resonant Microwave Cavity Across Furnace Back pass or Economizer Ductwork
- Total Ash Loading Determined by “Dust Probe”

Receiver Measures Microwave Intensity (Carbon)
Microwave Oscillator 94 GHz ± 75 MHz
Dust Probes (Loading)

CIA Output
Carbon/Ash Loading @ %
OR
Carbon @ g/m³
Carbon In Ash Instrument Installation

One microwave sender and receiver required per CIA unit
Carbon In Ash Instrument
Benefits

**Increased**
- Increased combustion efficiency
- Increased quality of Fly Ash resulting in better sale price!
- Improved Mercury capture
- Loss of Ignition availability
- Balanced plant efficiency

**Reduced**
- Reduced operating cost
- Reduced amount of Fly Ash & reduced Land Filling
- Reduced manual LOI procedure

ABB’s Carbon in Ash Instrument
OPTIMAX® Performance
Mill Run Back Calculator

- Run-Back Calculator based on physical model of the mill
- Outputs:
  - Maximal Drying capacity
  - Maximal grinding capacity
  - Moisture of coal / biomass
- Implemented on controller

Referenz:
P. Niemczyk et al: Derivation and validation of a coal mill model for control
OPTIMAX® Performance
Mill Drying capacity

- MCF: Max. coal/biomass addition
- 3:30: Addition of Biomass
Combustion Optimization Principe

- Targets
- Constraints

- Optimized setpoints

- Sum of weighted goals = minimum

- Optimizer

- Iteration

- Boiler model

- Measured values

- Controlled entities

- Optimized values
Combustion Optimizer
Typical Scope

- NOx – maximum constraint, main objective
- Opacity – maximum constraint, noisy value
- O2 imbalance – delta O2 between furnaces, controlled with furnace biases on Aux Air and OFAD
- Actuator constraints – must keep base DCS loops in operating range, usually below a max output
  - Spray valves
  - Dampers
Combustion Optimizer
Reference: reducing NOx

- Max limit lowered sequentially by 10 ppm from 225 to 195
Lifetime Monitoring
Motivation

**Boilers**
- Increasing peak operation results in additional load cycles on individual components
- New component materials allow higher steam parameters
- Optimum plant or boiler operation is achieved when the:
  - Operation is safe, and when there is
  - Good Agreement between design and the current operating lifetime consumption

**Turbines**
- Requirement for operational safety and high availability
- Obligation to prevent highly stressed components from failing,
  - due to:
    - Permanent loads such as high pressures and temperatures
    - Centrifugal forces in a high temperature range
    - Low-frequency alternating loads
Lifetime Monitoring
Boiler and Turbine

Features
- Online calculation of lifetime consumption of critical components
- BoilerLife certified by TÜV
- Calculations according to international standards
- Online reporting on lifetime status of critical components

Benefits
- Improving maintenance planning
- Ensure that components will not fail or need replacement too early
- Certified reporting to safety authorities
Soot Blowing Optimization
Model based calculation of heat exchangers

Activation signals for individual soot blower groups are:

- Temperature limits
- Soot blower steam consumption
- Water consumption of water injectors
- Boiler efficiency
- Injection rates of intermediate superheaters
- Pressure losses
- Blower performance
Soot Blowing Optimization
Calculation results with a detailed boiler model

Features
- Provides operator guidance as to when to initiate a soot blowing sequence
- Calculates cleanliness factors per section
- Measures heat transfer efficiency
- Applies to furnace, walls and convective sections

Benefits
- Easy-to-spot effects of minor changes in soot blowing sequences
- Significant heat rate savings
- Increase in long term plant performance
- Online computation of surface cleanliness
- Typical payback time < 2 years

![Graph showing calculated conditions of heat exchange areas and start of soot blowing sequence.](image-url)
BoilerMax
Boiler start-up Optimization

Benefits:
- Shorter start-up and shut-down time reduces fuel consumption
- Faster load response to load dispatcher, advantages in energy trading
- Explicit consideration of thermal stresses in thick-walled components, control of temperature variances during start-up
- Earlier warm-up and speed-up of the steam turbine and therefore earlier grid synchronization possible
BoilerMax
Functional principle

Power plant boiler

Nonlinear Model Predictive Control (NMPC) with cyclic tracking of the real process

- Boiler model
- Optimizer
- Optimization aims

- manipulated values
- optimized values
- Cost function = Minimum!
- Optimized setpoints and inputs

Optimization aims
Determination of thermal stresses

Principle:
- Temperature difference $\Delta T$ is indicator for thermal stresses
- Measurement of $\Delta T$ between inner surface and the mean diameter of the annular cross section of thick-walled components
- Alternative 1: determination on non-heated surface
- Alternative 2: indirect determination from steam temperature gradients

$\Delta T \approx T_m - T_i$
BoilerMax
Enhanced start-up phase

- Traditional start-up to comply with design limits
- BoilerMax start-up allows exploitation of design limits for more efficient process control:
  - Based on process model
  - NMPC technology
  - Predictive coordination of multiple variables
  - Online optimization in real-time

Up to 15% savings due to fast and low-stress boiler start-up
State Space Controller
Improved Temperature Control
State Space Controller
Improved Temperature Control

- Increasing the live steam and reheated steam operation temperature results in an immediate increment of unit efficiency
- With a higher set point, however, the margin between the operation point and max. admissible temperature is reduced
- This is no problem thanks to the improved performance that the state controller delivers
OPTIMAX® State Space Controller
Improved Temperature Control

PI-PI

State Space Controller (SSC)

Physical Limit
DCS Limit

PI-PI SP

Potential live steam temperature increase
Life Steam Flow Calculation
Reduction of Throttling Losses

live steam flow calculation (ABB patent)

Estimated value \( \hat{\dot{m}}_{LS} \)

\( T_{LS} \quad p_{LS} \)

\( \Delta p \)

\( p_{cold \; RH} \quad p_{HP} \quad T_{LS} \)

HP-bypass

Turbine inlet control valves
Unit Control
Flexible and Reliable Operation

MODAN:
Modified sliding pressure by turbine valve throttling

CONDSTOP:
Fast shutdown of the LP FW heater line on steam and condensate side

MODAKOND:
Modified sliding pressure by turbine valve throttling and LP heater line shutdown

Dynamic, Controlled Runbacks

Dynamic Load Model
Feedforward Turbine

Feedforward Boiler

Dyn. Pressure Model

Pressure Control

Fuel Controller

Load Dispatch

Unit SP

Frequency demand

Dyn. Pressure

Mddel

Feedforward

Boiler

Dynamic Model

Feedforward Turbine

ABB-CONDSTOP

MODAN:
Modified sliding pressure by turbine valve throttling

MODAKOND:
Modified sliding pressure by turbine valve throttling and LP heater line shutdown

CONDSTOP:
Fast shutdown of the LP FW heater line on steam and condensate side

Stationäre Turbinenandrosselung in %

Last in %

0 40 70 100

40 70 100

0

6

12

15

18
Energy Optimizer

- Flexible exploitation of different production units
  - Gas turbines
  - Boilers
  - Steam turbines
  - Different fuels
- Varying operational policies:
  - Prio steam production
  - Prio el. production
  - Start/Stop of boilers and turbines
- Energy Optimizer: Online-Optimization considering process constraints and market needs
Reference 1: Internal Optimization Jänschwalde
Pooling of six 500 MW units

Advantage of Multi-unit optimization
- Exploit communication network between management system and unit control system
- Real-time optimization of set points and secondary frequency control
- Fast and optimal reaction to fulfill production task, incl. gradients and timing of load ramps
- Goals:
  - minimize fuel consumption and CO₂-emissions
  - increase flexibility
Reference 2: Pooling of up to 500 biogas plants

Process Database
Redundant Controller
IEC 60870-5-104 Scanner
Operation & Management

Up to 500 production units, typically 500 kW per unit

Service Client
Operations Client
Engineering Client
Import / Export for operational management
Process values alone usually give no information about the efficiency or the process quality of a plant.
OPTIMAX® Plant Performance
Determination of Performance Indicators

- Performance indicators are determined by using multiple process values
OPTIMAX® PlantPerformance
Identifying the origin of a performance deviation
Loop Auditing

- Transparent commissioning of control through loop optimizer.
- Model based tuning of each individual loop with a well documented report for each loop.
- Reports are available at any time during commissioning giving a fast and accurate account of the loop commissioning status.
- Fully integrated into the System 800xA.
Loop Auditing

- Loop auditing given feedback on current control loop performance to detect worsening control loop behavior.
- Indicating possible causes for the worsening of the control loop performance.

Diagram:

- Loop Reports
- Causes
- Optimize Loops

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Power and Water Plant Operations
ABB Industrial Energy Efficiency (IEE) Assessment
Industrial Energy Efficiency (IEE)
Master Plan
Industrial Energy Efficiency (IEE)
Implementation

Industrial Energy Efficiency

Opportunity Identification | Master Plan | Implementation

- ABB Programme Manager
- ABB Energy Team
- ABB Engineering
- ABB Service
- ABB Automation & Technologies

- MANAGEMENT
- EXPERTISE
- ENGINEERING
- EXECUTION
- TECHNOLOGY

- Client Sponsor
- Client Energy Team
- Client Engineering
- Client Contractor
- 3rd Party/OEM Technologies